

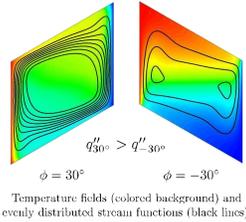
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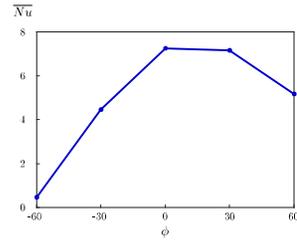
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Context

- In closed fluid cavities, the natural convection driven by the temperature difference between vertical hot and cold walls has been investigated in numerous occasions.
- The heat transfer is much more important when the vertical hot wall is located below the cold one (left cavity in the figure), compared to a case for which the vertical hot wall is located above the cold one (right cavity in the figure).
- This phenomenon is referred to as the **thermal diode potential**.
- The objective of this study is to investigate the thermal diode potential of air-filled enclosures when the three modes of heat transfer are considered.

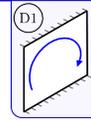


Pure-Convection Cavity

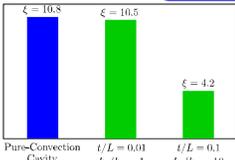
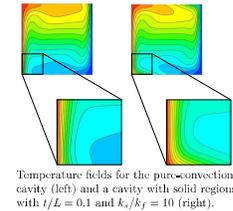
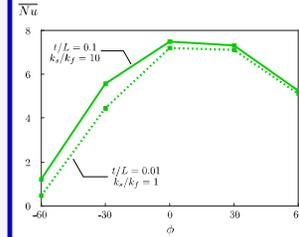


High asymmetry around $\phi = 0^\circ$:

High thermal diode potential ($\xi = 10.8$).



Convection-Conduction Cavity

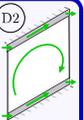


Convection-conduction vs. Pure convection

Slight increase of the Nusselt numbers.

Decrease of the temperature gradients in the fluid near the vertical walls;
Decrease of the convection heat transfer.

Moderate decrease of the thermal diode potential.



Methodology

- Finite-volume CFD simulations;
- 2D, laminar and steady;
- Mesh ranging from 22 500 to 40 500 elements;
- 2nd order schemes;
- Single adiabatic enclosures with or without solid regions.

Analysis parameters:

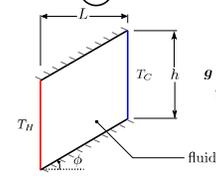
- Nusselt number:
$$\overline{Nu} = \frac{q''}{q''_{ref}} = \frac{q''}{k_f(T_H - T_C)/L}$$
- Thermal diode parameter:
$$\xi = \frac{\overline{Nu}|_{\phi=60^\circ}}{\overline{Nu}|_{\phi=-60^\circ}}$$

Governing dimensionless parameters tested:

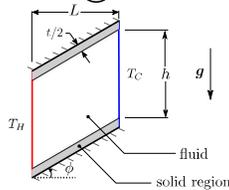
- | | | |
|------------------------------------|---|--------------------------------------|
| • h/L | 1 | Aspect ratio of the cavity |
| • Ra | $5 \cdot 10^5$ | Rayleigh number |
| • Pr | 0.71 | Prandtl number |
| • ϕ | $-60^\circ, -30^\circ, 0^\circ, 30^\circ, 60^\circ$ | Inclination angle |
| • t/L | 0.01, 0.1 | Thickness ratio of the solid regions |
| • k_{solid}/k_{fluid} | 1, 10 | Thermal conductivity ratio |
| • ϵ | 0.1, 0.9 | Uniform internal surface emissivity |
| • $\frac{T_H + T_C}{2(T_H - T_C)}$ | 9.75 | Radiation mean temperature |

Calculation domains:

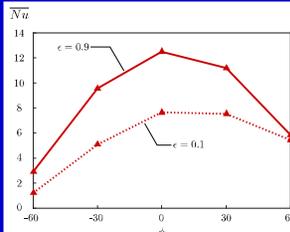
• Domain (D1):



• Domain (D2):



Convection-Radiation Cavity

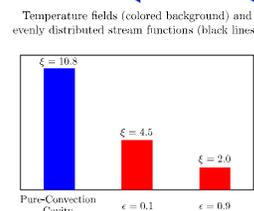
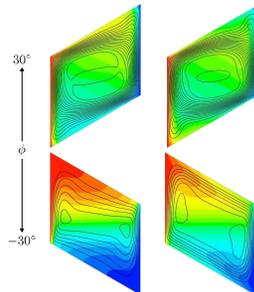


Convection-radiation vs. Pure convection

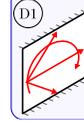
Important increase of the Nusselt numbers.

If ϵ increases:

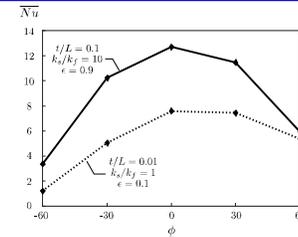
- For $\phi > 0^\circ$:
Large decrease of the convection heat transfer.
- For $\phi < 0^\circ$:
Small increase of the convection heat transfer.



Drastic decrease of the thermal diode potential.



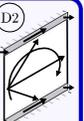
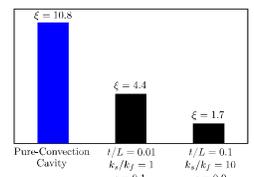
Three-Mode Heat Transfer Cavity



Three-mode heat transfer vs. Pure convection

Important increase of the Nusselt numbers.

Further decrease of the thermal diode potential.



Conclusion

- Due to the overall increase of the heat transfer and to the important interaction between the three modes of heat transfer, the thermal diode potential of parallelogrammic air-filled enclosures is significantly reduced when the three heat transfer modes are considered.
- For more details, see *The thermal diode and insulating potentials of a vertical stack of parallelogrammic air-filled enclosures*, to appear in the International Journal of Heat and Mass Transfer.

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